Carboxen[®] Synthetic Carbon Adsorbents for Host Cell Protein Removal During Monoclonal Antibody Purification

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Introduction

Monoclonal antibodies (mAbs) are a class of critical biotherapeutic drugs. The demand for mAbs is steadily increasing while the depletion of host cell proteins (HCP) in the manufacturing of mAbs remains a challenge. HCPs can represent an immune response risk after the administration of mAbs if not reduced to appropriate levels. Removal of HCPs is typically done via a Protein A (PA) chromatography capture step, which is carried out in a bind-andelute mode. Following the Protein A purification step, the feed is passed through two polishing steps in the form of ion exchangers (IEX), namely cation exchange chromatography (CEX) and anion exchange chromatography (AEX). Remaining impurities are mostly low molecular weight, hydrophobic HCPs that are difficult to remove because of their physiochemical properties (Wang et al. 2009)¹, or their non-specific association with the antibody (Shukla and Hinckley 2008)². They represent the group of critical HCPs which needs to be addressed to achieve the highest possible purification.

Efforts to further reduce HCP content beyond that achieved with the standard PA-IEX downstream processes are being considered. One such solution is to add additional polishing steps like hydrophobic interaction chromatography (HIC) between the PA and IEX chromatographic steps. In this work a post-Protein A (PPA) pool was applied to three different carbonbased adsorbents in flow-through mode to test their HCP depletion behavior under dynamic conditions.

Methods and Materials

Post Protein A Pool

The PPA pool was produced by treating a clarified cell culture harvest of CHO-K1 containing mAb02 with Protein A chromatography. For this purpose, a 205 x 26 mm (108 mL) column packed with ProSep[®] Ultra Plus Protein A resin was used on an Äkta[™] Pure 25 system. A high salt wash is typically applied to further reduce the HCP content; however, the salt wash was omitted here to keep the HCP content high for the purpose of challenging the adsorbents. The HCP content of the PPA used in this study was 6,000 ppm. After thirty minutes of virus inactivation the PPA pool was titrated to pH 5 with 2 M Tris(hydroxymethyl)aminomethane.

Adsorbent Materials

Two Carboxen[®] synthetic carbon adsorbents and a commercially available depth filter were investigated for their HCP removal capability and mAb recovery. Carboxen[®] 1032 and Carboxen[®] 569 are commercially available (Merck KGaA, Darmstadt, Germany) synthetic carbon adsorbents with particle sizes in the range of 20-40 mesh. For this study, customized 50 µm particles of these two synthetic carbons were used. The depth filter was selected for comparative purposes. The depth filter adsorbent bed is comprised of traditional naturally sourced activated carbon and cellulose.



A scanning electron micrograph of the synthetic carbon particles is shown in **Figure 1**. The synthetic carbons are highly engineered derivatized resins. They have been designed to withstand high pressures, up to 110 MPa. Resins used in bio-chromatography would undergo plastic deformation and traditional activated carbons are known to fracture and generate fines at far lower pressures.

Functionalization of carbon surfaces with oxygen functional groups alters the materials' pH and hydrophobic/hydrophilic properties. The pH of



Figure 1. Scanning electron micrograph of 50 μm Carboxen® Synthetic Carbon.

Carboxen[®] synthetic carbons can be tailored from 2.5 to 10.5. The pH can be selected to meet the application needs. The surface chemistry dictates the hydrophobic/ hydrophilic properties and with proper oxygen functionalization the synthetic carbon adsorbent can be anywhere from hydrophilic to extremely hydrophobic. The Carboxen[®] synthetic carbons are activated through physical means. Therefore, there is no chemical residual left on the carbon that could create a chemical leaching concern in use. They are of high purity and pass all the extractable and leachable tests as outlined in both USP 43 - NF 38 and Ph. Eur 10. As they are produced from a synthetic source, Carboxen[®] synthetic carbons are inherently free of heavy metals and other inorganic content found in naturally derived adsorbents.

While eight Carboxen[®] synthetic carbons are commercially available, 1032 and 569 were particularly selected since their properties are markedly different and thus a performance difference was anticipated between the two. Carboxen[®] 569 is highly hydrophobic and does not contain any ligand or attached surface functionality, and it can be thought of as a super phenyl phase. Carboxen[®] 569 has a point of zero charge at pH 8.8. Carboxen[®] 1032 is functionalized with oxygen surface functional groups that give the material more of a hydrophilic character and a point of zero charge at pH 4.1. Material properties of the eight commercially available materials are given in **Table 1**.

				Pore Structure (%)			
	Surface Area (m²/g)	Surface pH (ASTM D6851)	1 = most hydrophilic 10 = most hydrophobic	Micro (< 20Å)	Meso (20 - 500Å)	Macro (>500Å)	Ball Pan Hardness (ASTM D3802)
Carboxen [®] 563	500	6.8	7	38	24	38	99.8
Carboxen [®] 564	400	8.7	8	47	26	27	99.8
Carboxen [®] 569	500	8.6	9	45	32	23	99.4
Carboxen [®] 572	1000	9.5	4	48	23	29	99.1
Carboxen® 1005	1000	8.0	10	47	26	27	99.6
Carboxen® 1032	800	3.0	1	49	0	51	98.6
Carboxen® 1033	400	7.0	3	38	0	62	99.7
Carboxen® 1034	1200	10.5	2	52	3	45	98.9

Table 1. Carboxen[®] Synthetic Carbon Material Properties

Experimental Procedure

The Carboxen[®] materials were packed into 300 µL Super Compact Columns (Götec Labortechnik GmbH, Germany). The columns' inner diameter was 5 mm and the bed depth, 1.5 cm. The depth filter was used directly. Prior to the purification process, the depth filter was flushed with Milli-Q[®] water for 100 L/m² and conditioned with 50 mM acetate buffer for 300 L/m² at a flux of 300 L/h/m², corresponding to 2.5 mL/min. Packed columns containing Carboxen[®] synthetic carbons were flushed and conditioned with 50 mM acetate buffer for 50 column volumes at a flow rate of 0.5 mL/min.

For the HCP removal analysis, a pre-defined volume of 200 mL of the PPA pool was applied to each adsorbent.

To maintain a residence time of 90 s within the devices, flow rates of 0.2 mL/min and 2 mL/min (corresponding to a flux of 240 L/h/m²) for the columns and the filter were applied, respectively. The PPA pool and each flow-through fraction were characterized by size exclusion chromatography (SEC) to determine the mAb load (onto each adsorbent) and mAb recovery. A Tosoh TSKgel[®] Super SW3000 SEC column was used on an Ultimate[™] 3000 UHPLC system with diode-array detector. HCP breakthrough was measured with ELISA. A CHO Host Cell Proteins 3rd generation ELISA-Assay Kit F550-1 from Cygnus Technologies was utilized. The procedure was carried out according to the manufacturer's instructions.

Results and Discussion

For comparison of the different adsorbents regarding their suitability for HCP depletion, the filter area was converted to volume based on its given dimensions. The HCP breakthrough was then plotted against the load of HCP (**Figure 2A**) and the load of mAb (**Figure 2B**) per adsorbent volume. Since the comparison was made at an HCP breakthrough of 10%, only this range is displayed.



Figure 2. HCP breakthrough plotted against A) load HCP and B) load of mAb per unit volume of adsorbent.

Carboxen[®] 1032 had the best performance among the three materials and showed a very good depletion of HCPs. At an HCP breakthrough of 10%, 2300 grams of mAb per liter of adsorbent could be applied on Carboxen[®] 1032 and 14 grams of HCP per liter of adsorbent could be depleted. The depth filter performed the worst among the three materials tested for HCP depletion, with a depletion of about 3 grams of HCP per liter of adsorbent after an application of 500 grams of mAb per liter of adsorbent. Carboxen[®] 569 showed a performance in-between that of the other two materials tested. On Carboxen[®] 569, 900 grams of mAb per liter of adsorbent could be applied, and 5 grams of HCP per liter of adsorbent could be depleted. All three materials tested had a high mAb recovery, upward of 95%.

Carboxen[®] 1032 is assumed to be slightly negatively charged at pH 5, as its point of zero charge is lower than pH 5. Considering the excellent HCP depletion obtained by this material, it is likely that most of the proteins are positively charged or uncharged under the given conditions. This leads to the assumption that most proteins have an isoelectric point of 5 or higher. In contrast, Carboxen[®] 569 is assumed to be strongly positively charged at pH 5 as it has a point of zero charge greater than pH 5. The depth filter contains activated carbon as adsorbent and is also likely to be positively charged at pH 5. Therefore, the positively charged proteins are repelled by these adsorbents.

Carboxen[®] 1032 worked best, out of all the materials investigated in this study, and under these specific conditions. However, PPA pools are highly variable as are the purification conditions (e.g. pH and conductivity) and the polishing media need to fit accordingly. There are eight commercially available Carboxen[®] synthetic carbons that cover a wide range of material properties with dispersion pHs ranging from 2.5 to 11 (Table 1), and from extremely hydrophobic to hydrophilic materials. Likely there is a Carboxen® synthetic carbon or a mixture that can optimize HCP depletion while maintaining high mAb yield in most mAb purification processes. This could be achieved by finding the best suited pH and conductivity for the PPA. For example, Carboxen[®] 569 is a strongly hydrophobic material. An increase in conductivity is expected to improve the HCP removal, as protein charges can be shielded by the added salt. Furthermore, pH variations could lead to different HCP depletion due to their different isoelectric points.

Conclusion

The Carboxen[®] synthetic carbons demonstrated excellent host cell protein reduction and high mAb yield. Carboxen[®] 1032 had the best performance among the three materials tested and showed a very good depletion of host cell proteins. At a HCP breakthrough of 10%, 2300 grams of monoclonal antibody per liter of adsorbent could be applied on Carboxen[®] 1032 and 14 grams of HCP per liter of adsorbent could be depleted. With the addition of a Carboxen[®] synthetic carbon polishing step to the standard PA-IEX downstream processes, difficult to remove lower molecular weight and hydrophobic HCPs can be depleted. With an added synthetic carbon purification step, downstream ion exchangers would bear a lower burden due to the reduction of impurities, so that their durability can be increased. Ideally, the implemented step can replace one of the downstream ion exchangers. These points would lead to a reduction in production costs. In an alternative configuration, the Carboxen[®] synthetic carbon can act as a final polishing step to target the critical HCPs that are not removed in the standard PA-IEX process. This can ultimately lead to the production of a safer mAb product for the patient.

References

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